

Modelling turbulent fluid-, thermo-, and droplet dynamics in the Leipzig Aerosol Cloud Interaction Simulator (LACIS-T)

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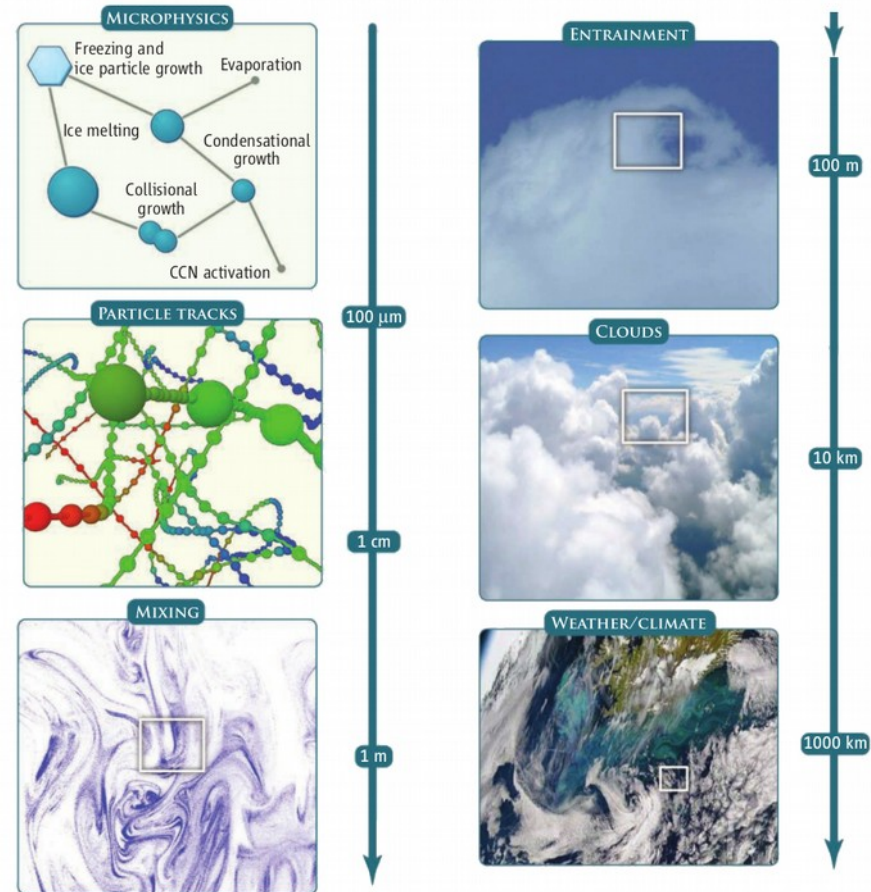
Outline

- 1 Introduction
- 2 Fluid and thermodynamics
- 3 Particle/droplet dynamics
- 4 Conclusions and outlook

1 Introduction

1 Introduction – Clouds

- Play a huge role in long term climate predictions as wells as in short term weather forecasts
- Hard to investigate
 - Transient, turbulent, intermittent, inhomogeneous
 - Wide range of spatial and temporal scales
 - Usually hard to reach
- Set up of a facility able to simulate clouds under reproducible conditions

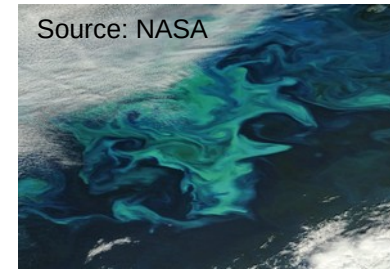
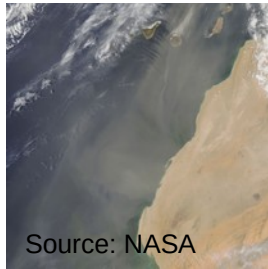


Source: Bodenschatz, E., Malinowski, S. P., Shaw, R. A., & Stratmann, F. (2010). Can we understand clouds without turbulence?. Science, 327(5968), 970-971.

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1 Introduction – Clouds

- Formed by water vapour, condensing at **cloud condensation nuclei**
- CCNs: Dust, black carbon, sulfate, phytoplankton, sodium chloride, ...

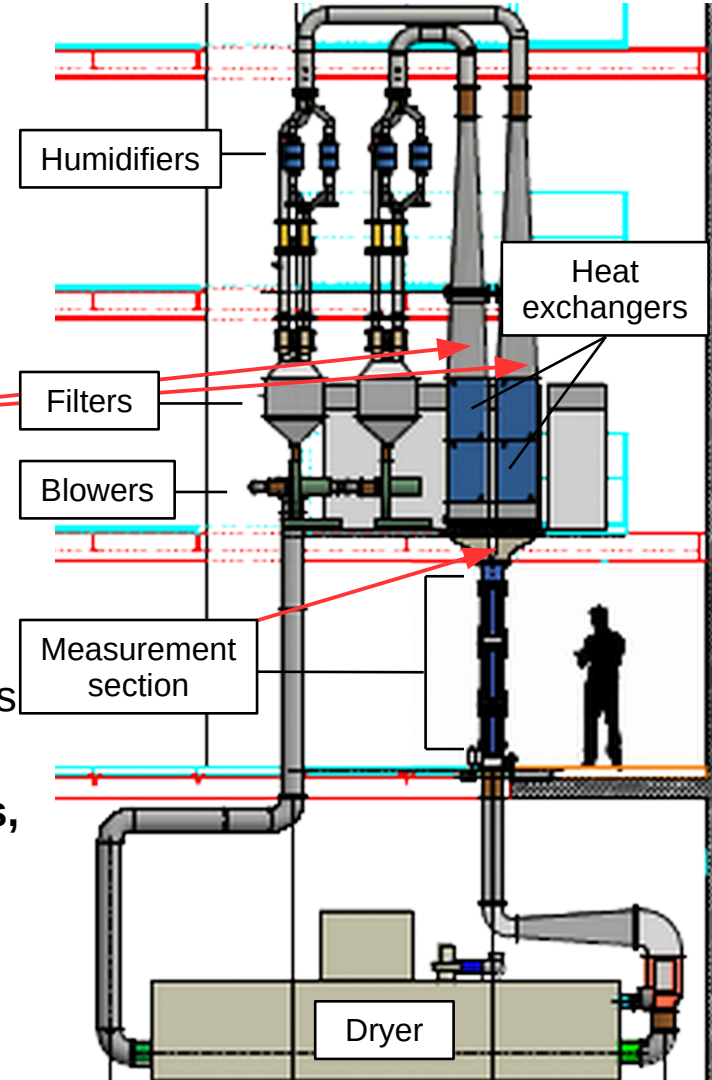


- Size range $\sim 0.1\mu\text{m}$
- Condensation determined by material, particle and ambient physical properties (especially temperature and water vapour content)
 - ➔ How much do turbulent fluctuations of ambient properties influence particle and droplet microphysics?

1 Introduction – LACIS-T

- Turbulent Leipzig Aerosol Cloud Interaction Simulator (LACIS-T)
- Closed-loop (Göttingen-type) wind tunnel
- Two branches, each with up to 5000 L/min
- Precisely defined thermodynamic and flow conditions
 - Velocity: up to 1.5m/s
 - Temperature and dew point: -40°C ... 25°C
- Injection of well defined particles between the branches

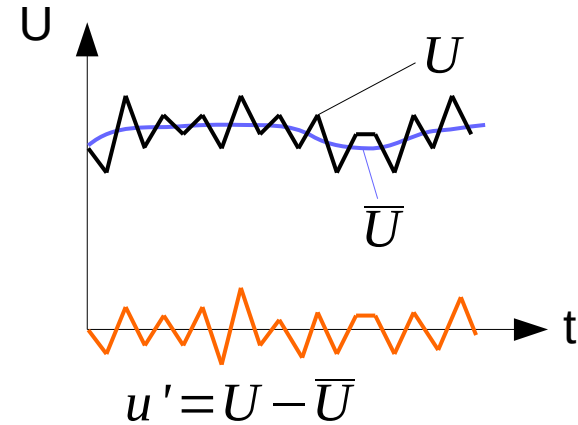
Are we able to simulate the flow, the thermodynamics, and particle/droplet behaviour inside LACIS-T?



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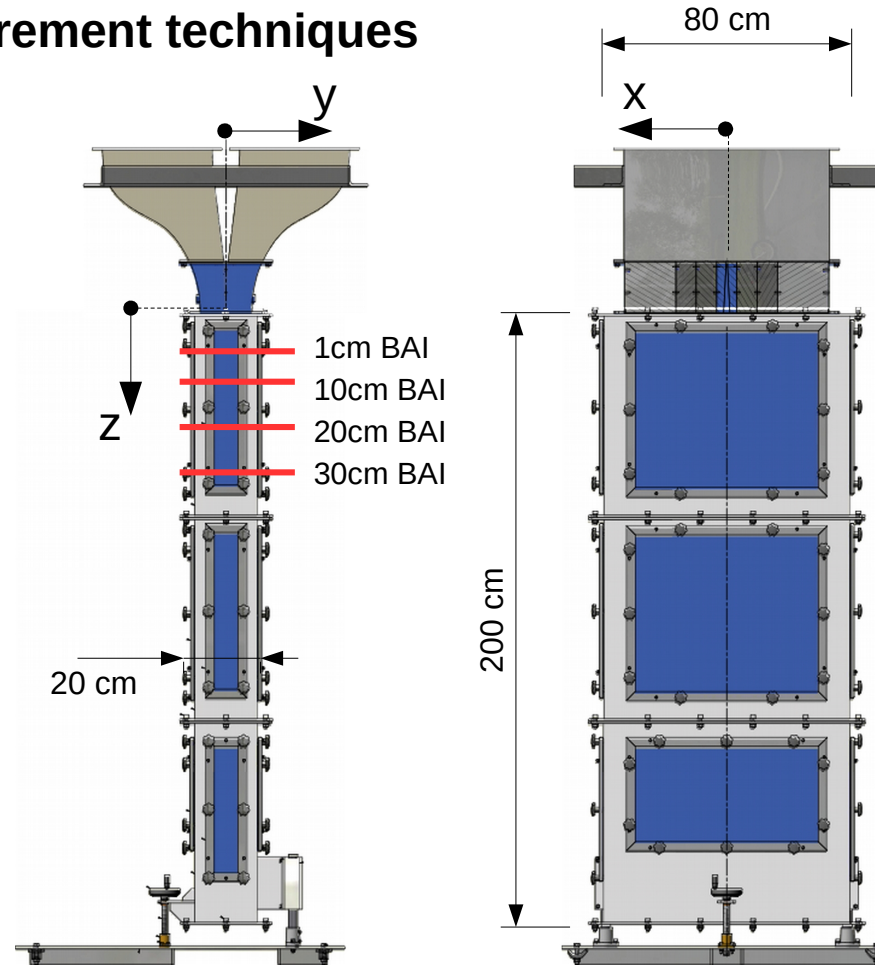
2 Fluid and thermodynamics

- Fields of instantaneous, mean and root mean square (RMS) values necessary for correlations between thermodynamic fluctuations and particle microphysics
- Measurement → Usually limited insight in flow and particle properties
- Simulation
- Exact knowledge of thermodynamic conditions necessary to simulate particle behaviour, including
 - Velocity and turbulence
 - Temperature
 - Humidity



2 Fluid and thermodynamics – Measurement techniques

- Point probes:
 - Hot wire anemometer (velocity)
 - Cold wire (temperature)
- On points along lines in y-direction in different heights below aerosol inlet (BAI) (z-axis)
- High frequency measurements (3kHz)
- Analysis gives mean and RMS value profiles



2 Fluid and thermodynamics – Numerical methods

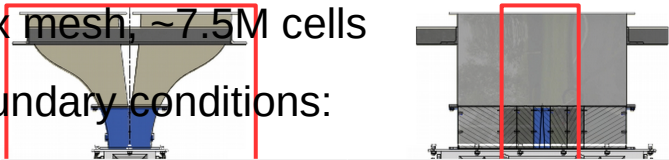
- Finite volume method with OpenFOAM
- Solving transient, incompressible Navier-Stokes-Equations
- PIMPLE-algorithm (merged PISO¹⁾ and SIMPLE²⁾), allowing larger time steps
- Solver “pimpleFOAM”
- Simulation of temperature with Boussinesq approximation and humidity as passive scalar
- 2nd order schemes (except divergence of k and $v_t \rightarrow$ limiter towards 1st order upwind)
- Considering turbulence with Large Eddy model (“dynamic k-equation”)
- Calculated 2.5s real time
- Statistics done for time after 0.5s (quasi steady flow reached)

¹⁾ Pressure Implicit Split Operator (transient)

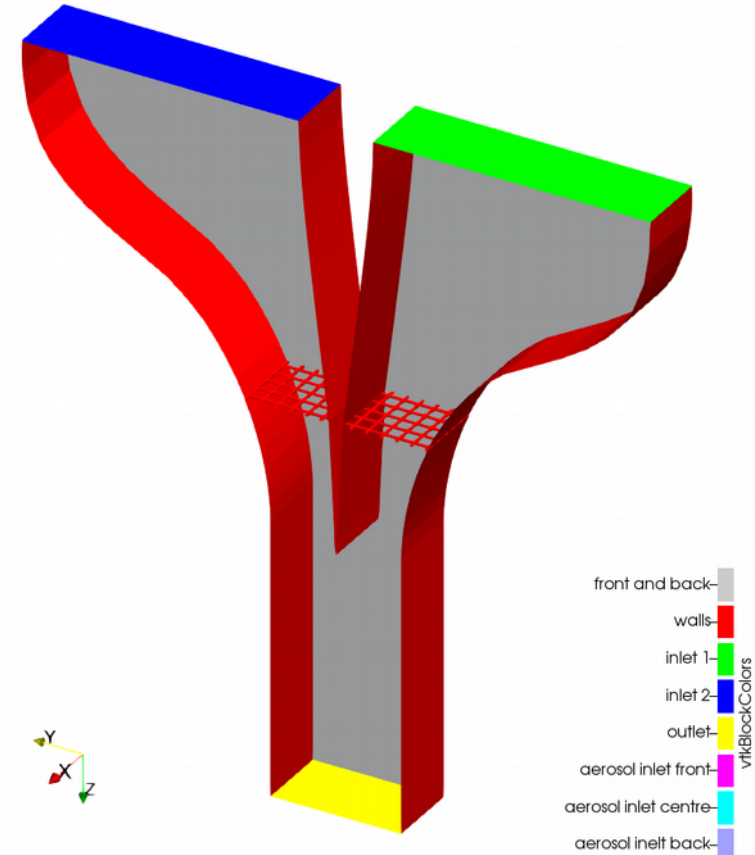
²⁾ Semi Implicit Method of Pressure Linked Equations (steady state)

2 Fluid and thermodynamics – Domain & Boundary Conditions

- Wind tunnel is modelled only partially
- Hex mesh, ~7.5M cells
- Boundary conditions:



	U	p	T & H
Inlet 1	$\begin{pmatrix} 0 \\ 0 \\ 0.39 \end{pmatrix}$	Zero gradient	Fixed value
Inlet 2			
Walls	0	Zero gradient	Fixed value
Outlet	Zero gradient	0	Zero gradient
Aerosol inlets	0	Zero gradient	Fixed value
Front and back	cyclic	cyclic	cyclic



2 Fluid and thermodynamics – Results – Velocity

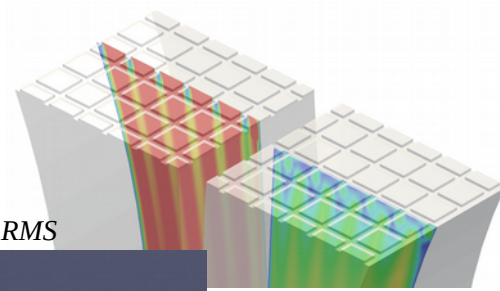
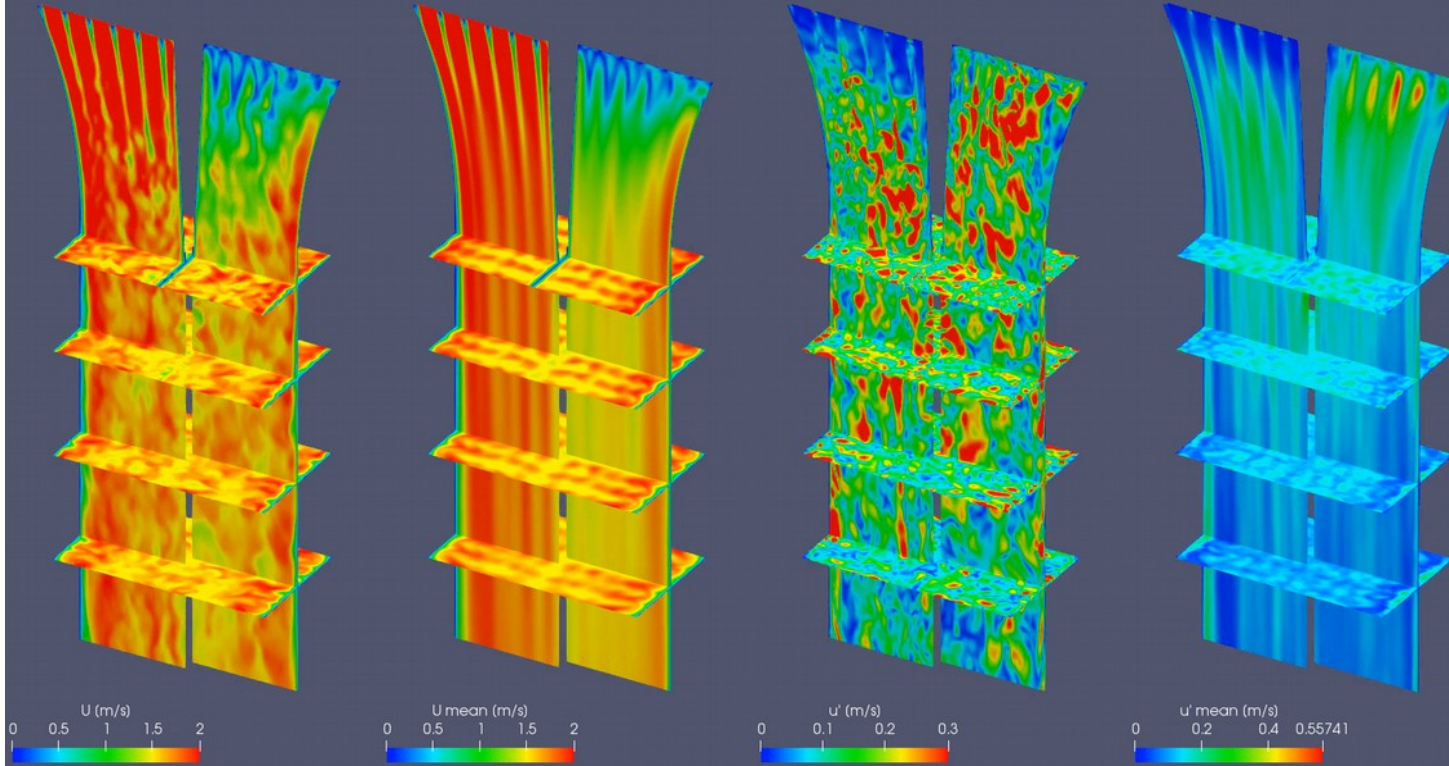
U_{inst}

\bar{U}

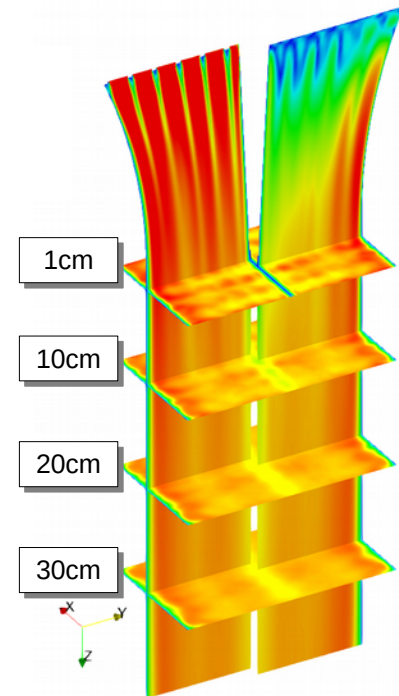
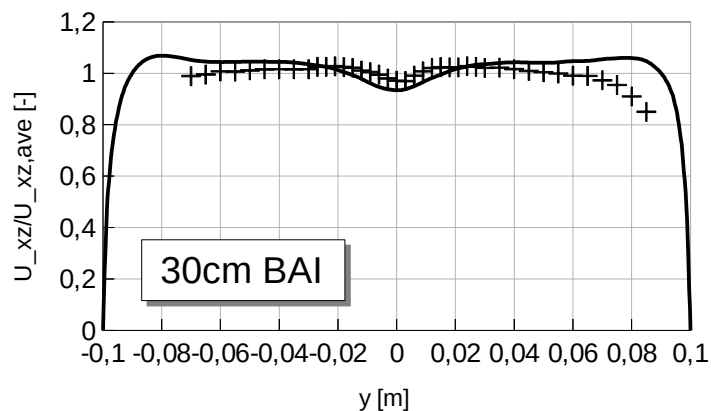
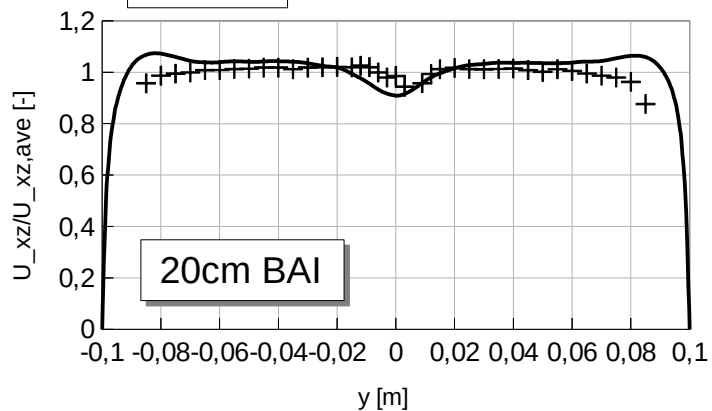
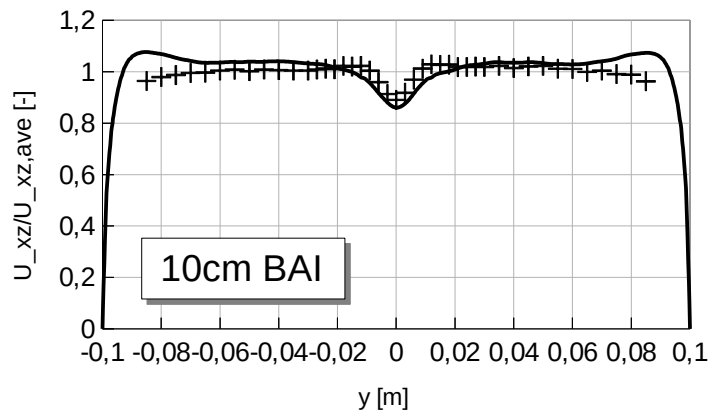
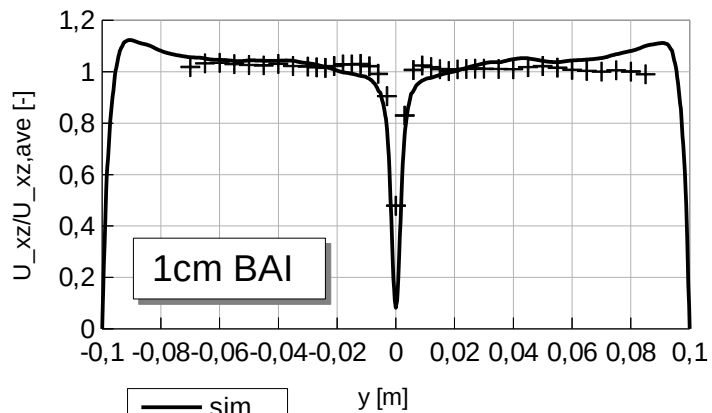
$u' = U_{inst} - \bar{U}$

u'_{RMS}

Time = 0.28 s



2 Fluid and thermodynamics – Results – Velocity



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2 Fluid and thermodynamics – Results – Turbulence

- Visualisation of turbulent structures with Q-iso-surfaces

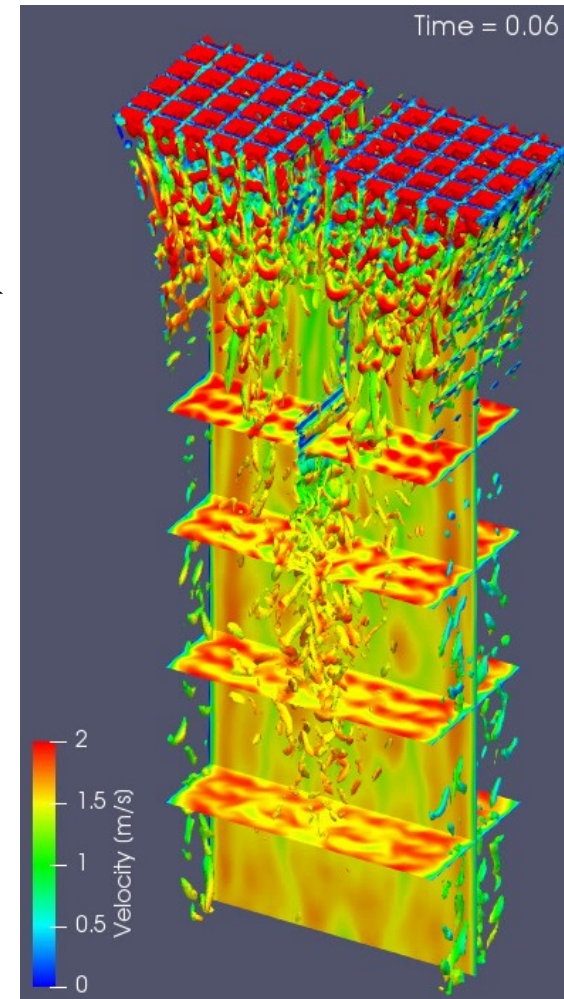
$$Q = \frac{1}{2} \left[(\text{tr}(\nabla \mathbf{U}))^2 - \text{tr}(\nabla \mathbf{U} \cdot \nabla \mathbf{U}) \right]$$

- Comparison to measurements with turbulent intensity

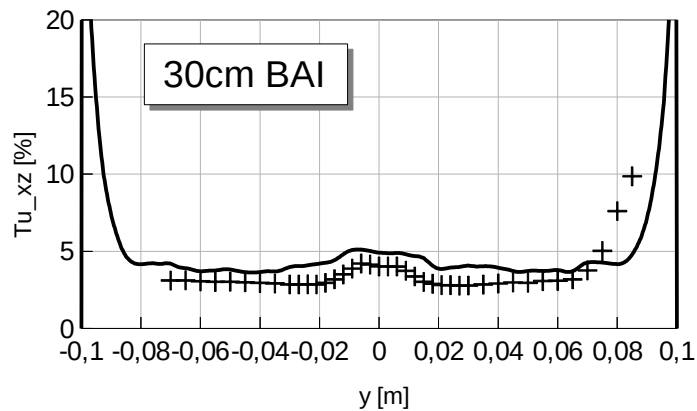
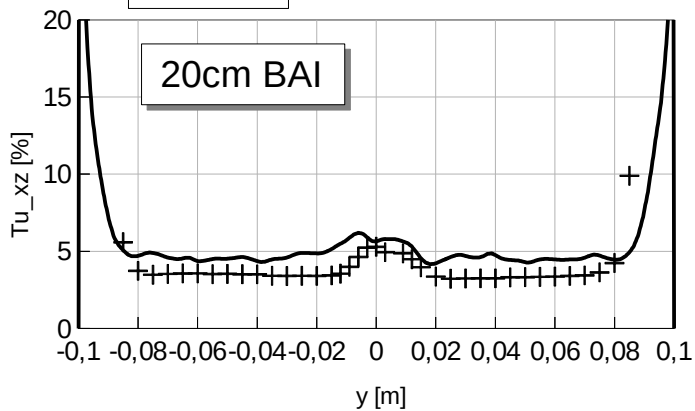
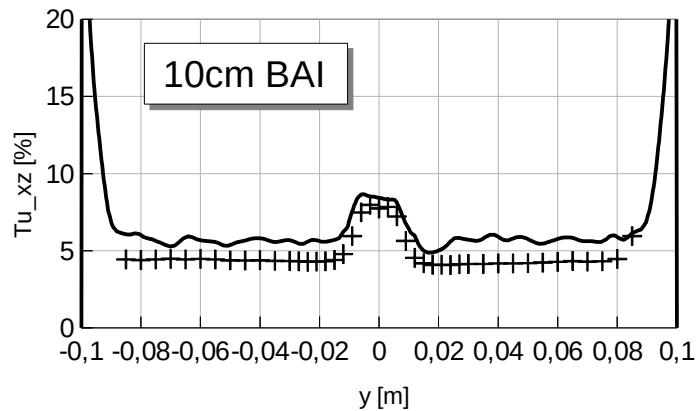
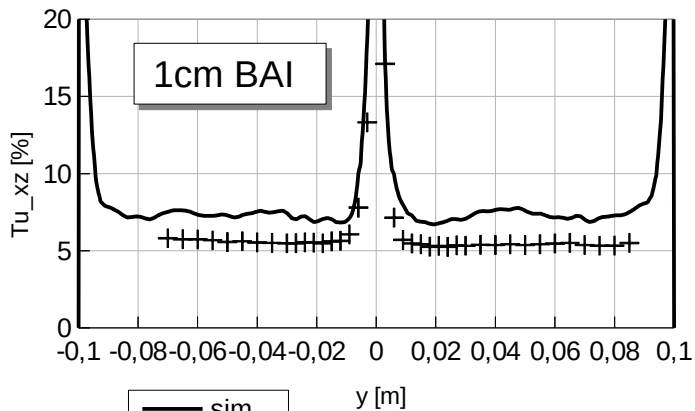
$$Tu = \frac{u'_{RMS}}{\bar{U}} = \frac{(\bar{U} - U)_{RMS}}{\bar{U}}$$

- Hot wire measures only two components, thus

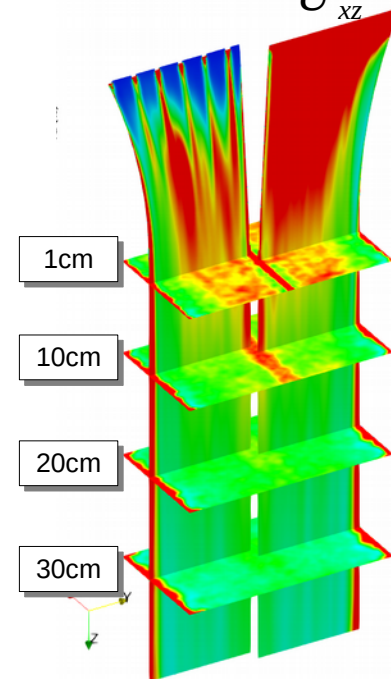
$$Tu = Tu_{xz} = \frac{u_{xz}'_{RMS}}{\bar{U}_{xz}} = \frac{(\bar{U}_{xz} - U_{xz})_{RMS}}{\bar{U}_{xz}}$$



2 Fluid and thermodynamics – Results – Turbulence



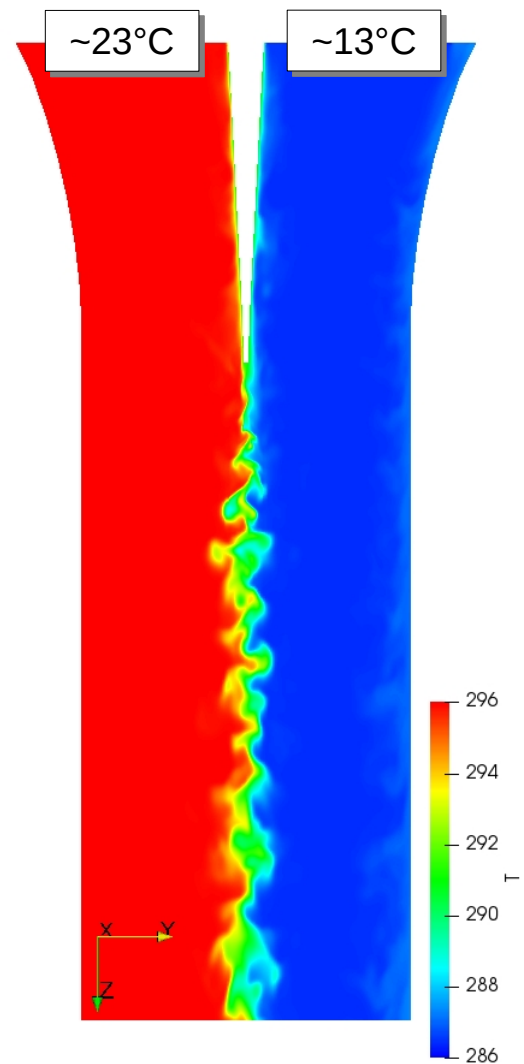
$$Tu_{xz} = \frac{u'_{xz} \text{ RMS}}{\bar{U}_{xz}}$$



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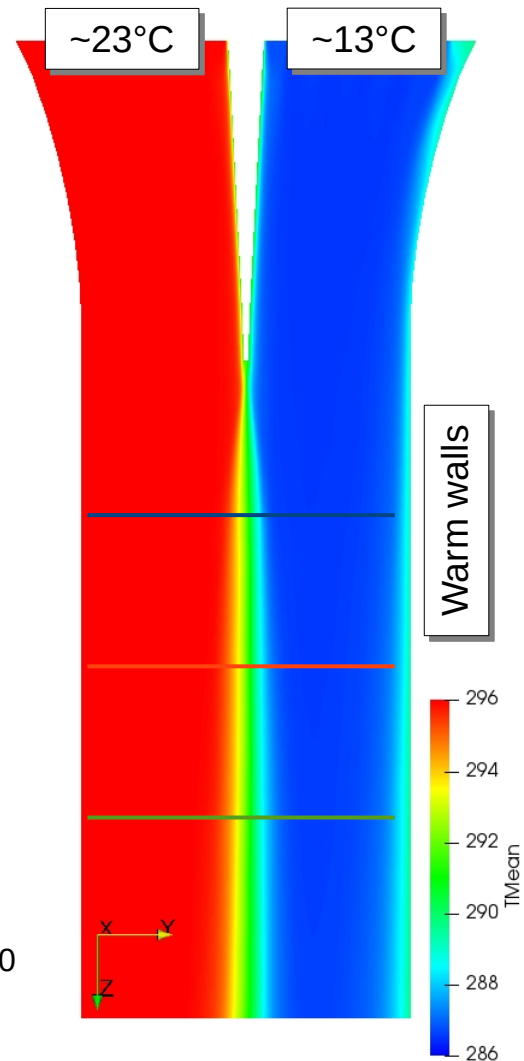
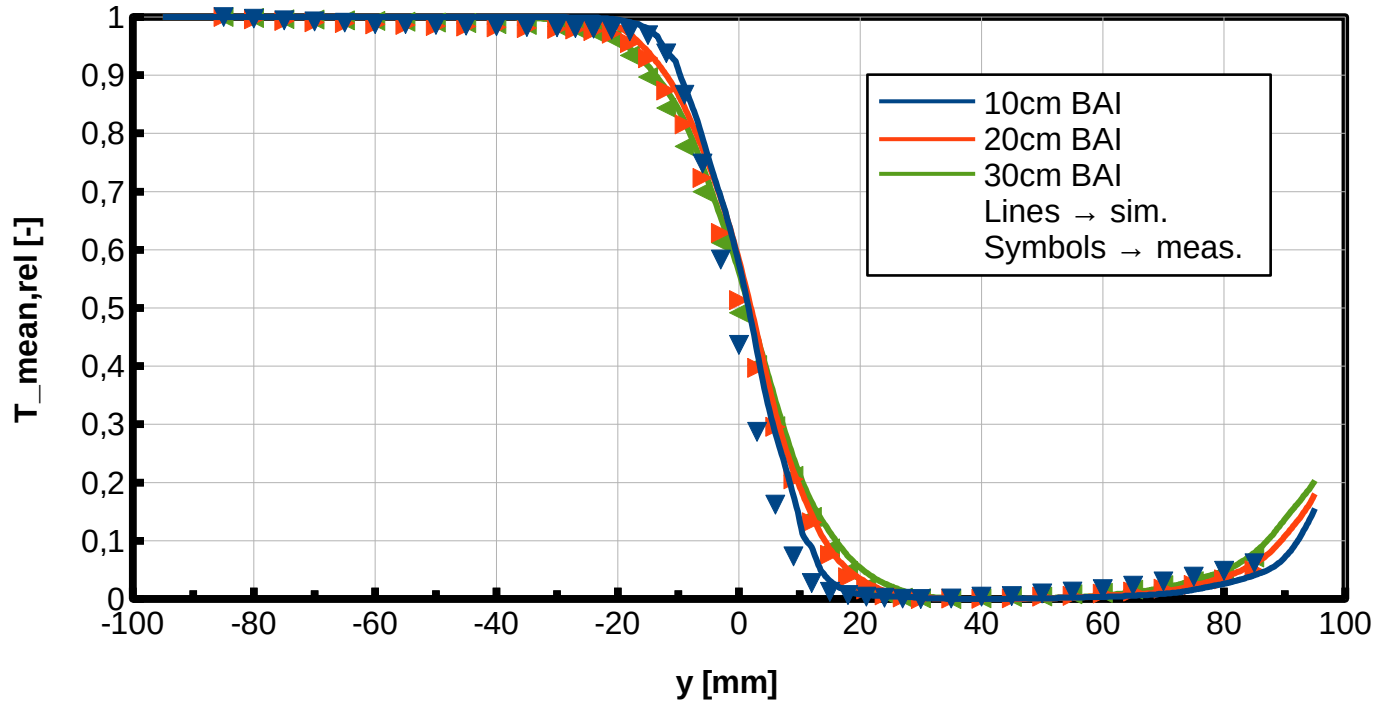
2 Fluid and thermodynamics – Results – Temperature

- Example: Mixing of warm and cold air below aerosol inlet



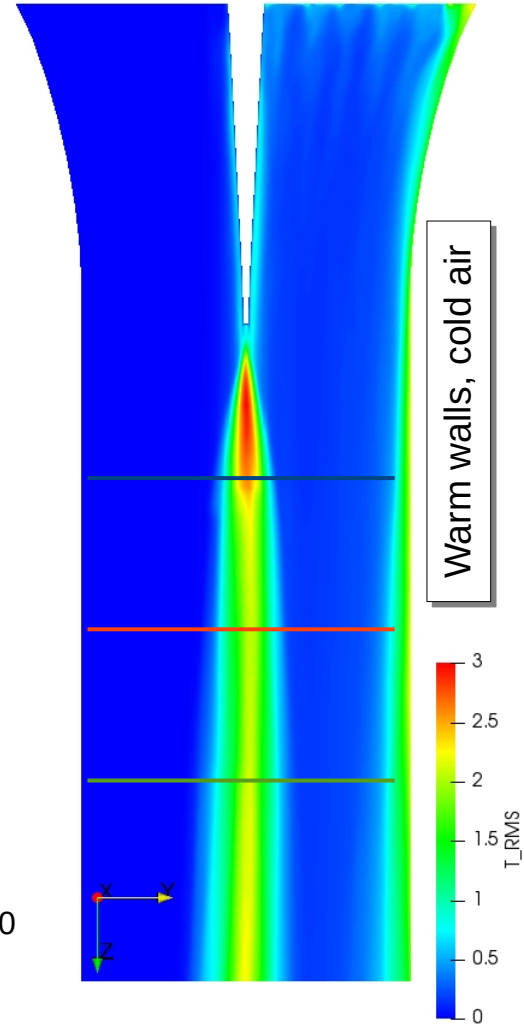
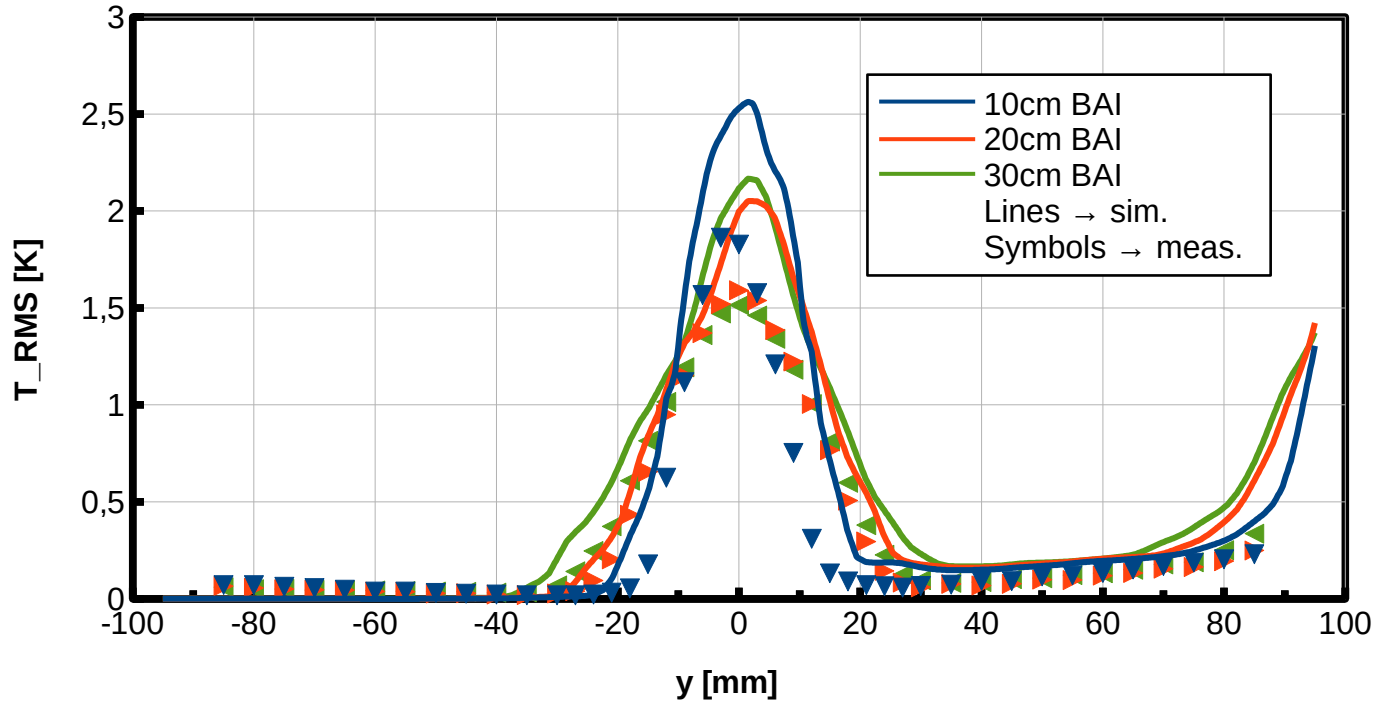
2 Fluid and thermodynamics – Results – Temperature

$$T_{mean,rel} = \frac{T_{mean} - \min(T_{Mean})}{\max(T_{Mean}) - \min(T_{Mean})} \rightarrow 0 \hat{=} T_{min}, 1 \hat{=} T_{max}$$

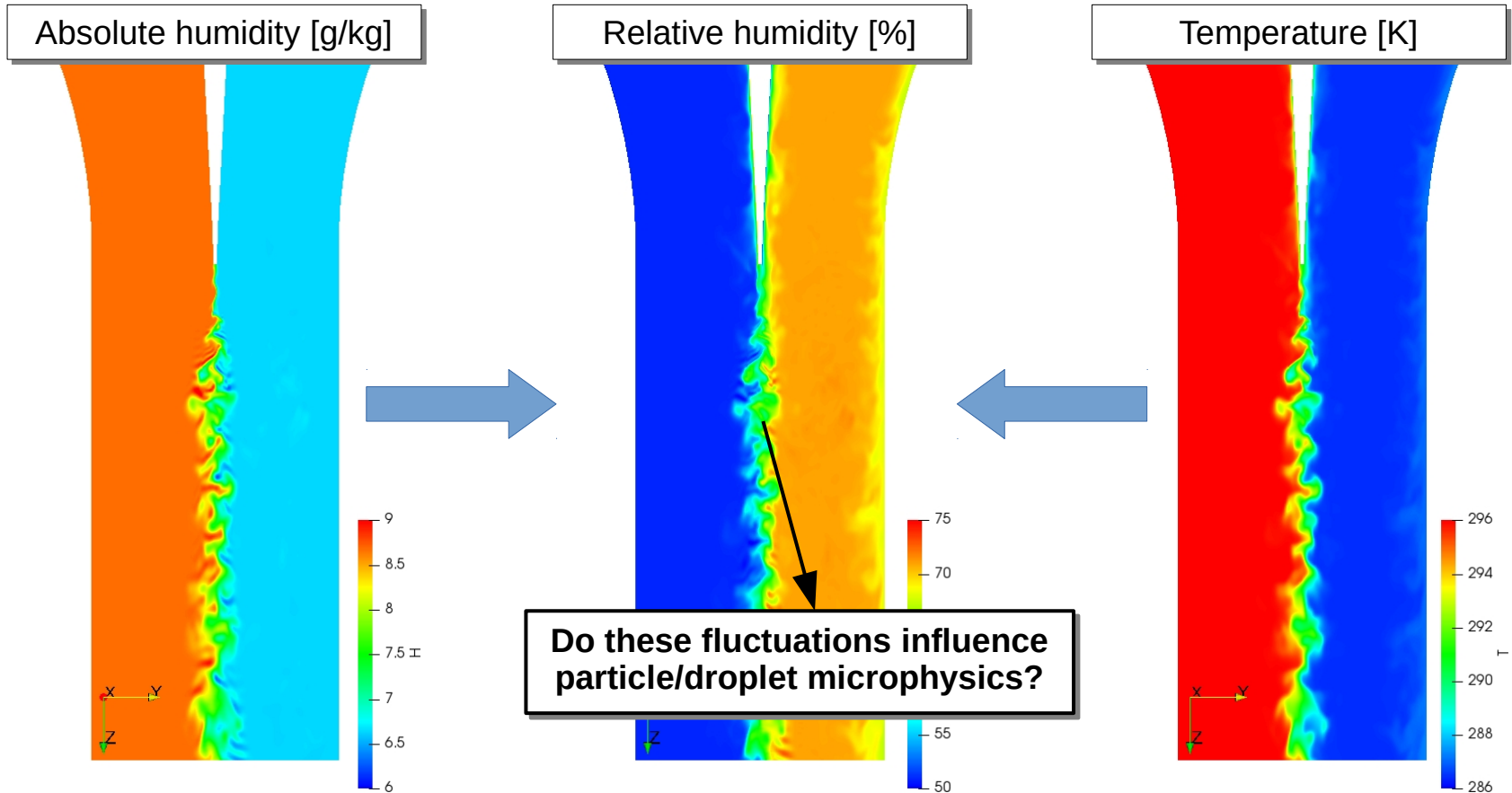


2 Fluid and thermodynamics – Results – Temperature

$$T_{RMS} = \sqrt{(T - T_{Mean})^2}$$

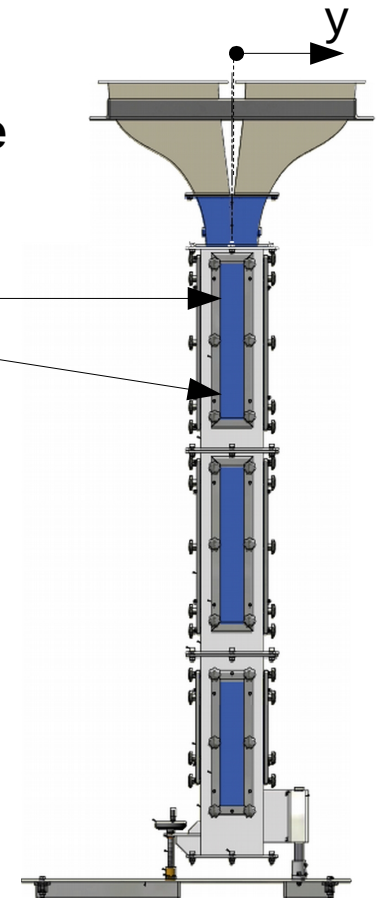


2 Fluid and thermodynamics – Results – Humidity



3 Particle and droplet dynamics – Measurement technique

- Usage of white light spectrometer WELAS from PALAS
- Measurement heights ~10cm BAI or ~35cm BAI
- Measuring particle diameter for 20 minutes
→ Particle size distribution

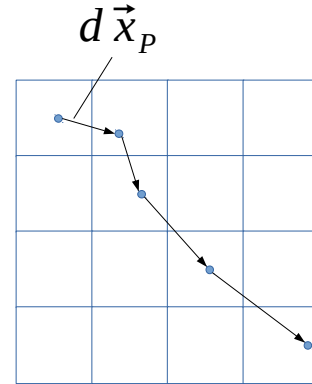


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3 Particle and droplet dynamics – Numerical method

- Tracking of individual particles (Lagrangian reference frame) through flow field (Eulerian reference frame)
- Assumption: point-mass-particles
 - Models for interactions with carrier fluid, other particles, electric fields, ...
- Particles usually approximated as spheres
- Particle size \ll size of control volume
- Trajectory calculation through 3 ODEs:

$$\begin{aligned} \frac{d\vec{x}_P}{dt} &= \vec{u}_P \\ m_P \frac{d\vec{u}_P}{dt} &= \sum_i \vec{F}_i \\ \left(I_P \frac{d\vec{\omega}_P}{dt} = \sum_i \vec{T}_i \right) \end{aligned}$$



3 Particle and droplet dynamics – Models

- Only drag force considered here
- Additional models:
 - Injection model (defining particle properties like position, size, and velocity at injection)
 - Growth/Mass transfer model

$$\frac{dm}{dt} = 2 \pi d_p \rho_{v, sat} (S - S^*) f_{mt}$$

- Mass transfer from gas phase to particles driven by gradient of water vapour saturation between particle surface and gas phase

Fluid data (fixed for Lagrangian time step):

- ρ Ambient pressure [Pa]
- T Ambient temperature [K]
- T_c Ambient temperature [$^{\circ}\text{C}$]
- H Mixing ratio [kg/kg]

Particle data:

- Variable:
 - d_p Particle diameter [m]
 - dt Lagrangian time step [s]
 - m_l Mass of liquid content [kg]
- Fixed:
 - m_s Mass of solid content [kg]
 - ρ_s Density of solid content [kg m^{-3}]
 - ρ_l Density of liquid content [kg m^{-3}]
 - sf Shape factor [-]

Model data (fixed):

- $dmRatio_{max}$ Maximum mass change ratio [-]
- D Vapour diffusivity in air [$\text{m}^2 \text{s}^{-1}$]
- M_l Molar mass of liquid content [kg mol^{-1}]
- M_s Molar mass of solid content [kg mol^{-1}]
- M_{dryAir} Molar mass of dry air [kg mol^{-1}]
- R Gas constant [$\text{J mol}^{-1} \text{K}^{-1}$]
- σ_l Surface tension of liquid [N m^{-2}]

Euler-Loop

Lagrange-Loop

Growth Model

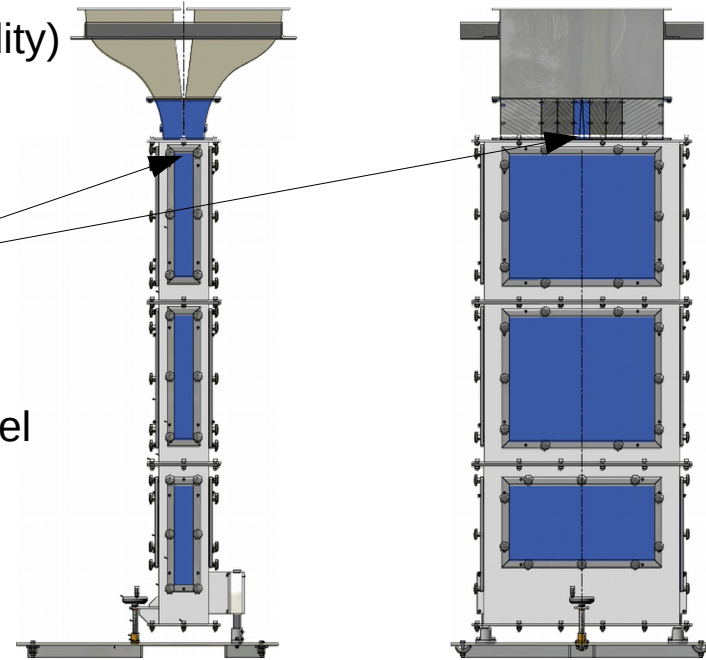
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3 Particle and droplet dynamics – Boundary conditions

- Two cases considered (high and medium relative humidity)
- Properties of sodium chloride particles
- Diameter of 320nm (mass equivalent to measurement)
- Injected at aerosol inlet between two branches
- Tracking time ~0.5s
- Sub time steps for Lagrangian tracking and growth model chosen automatically

$$Co_p \leq 0.5$$

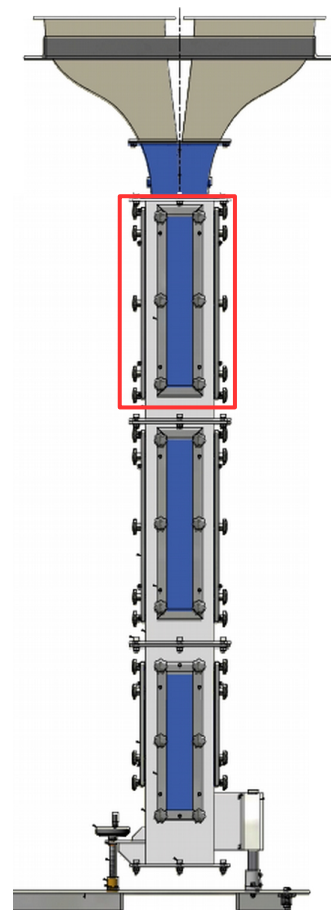
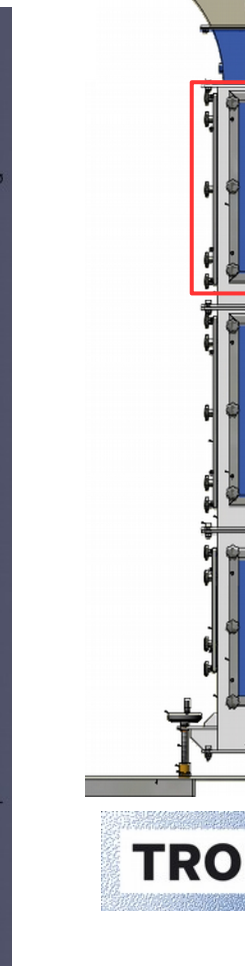
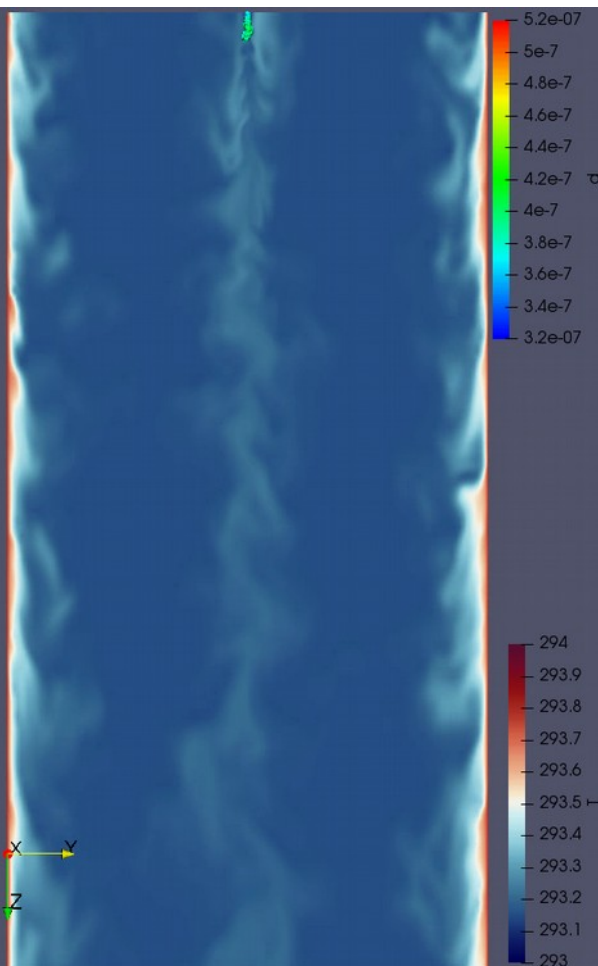
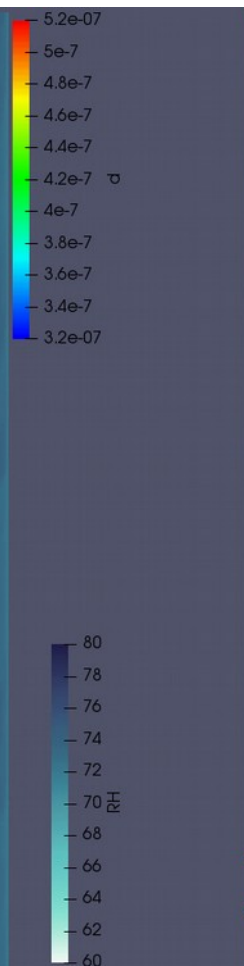
$$\frac{dm_p}{m_p} \leq 0.2$$



3 Particle and droplet dynamics – Results – Medium humidity

Relative humidity [%]

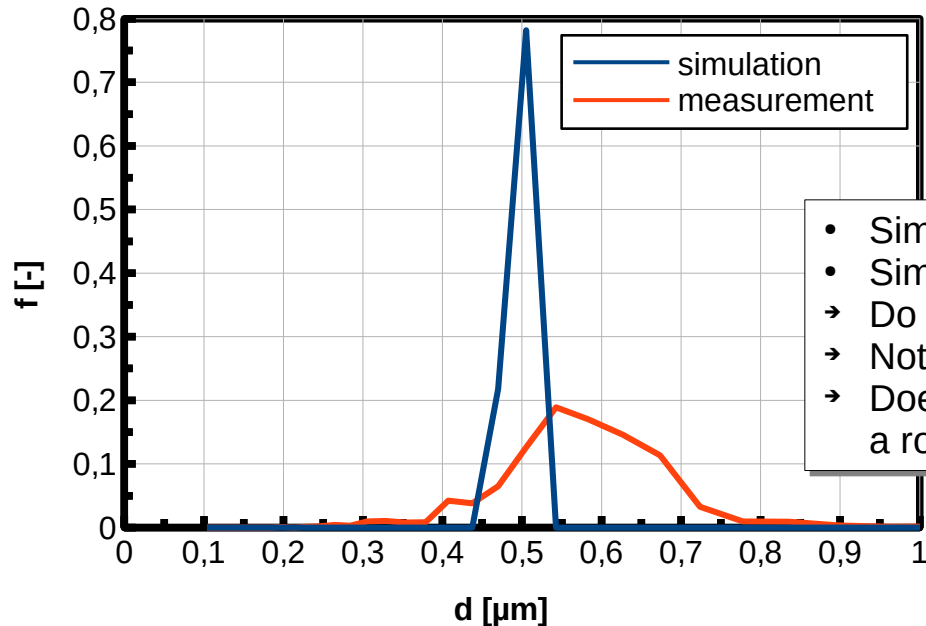
Temperature [K]



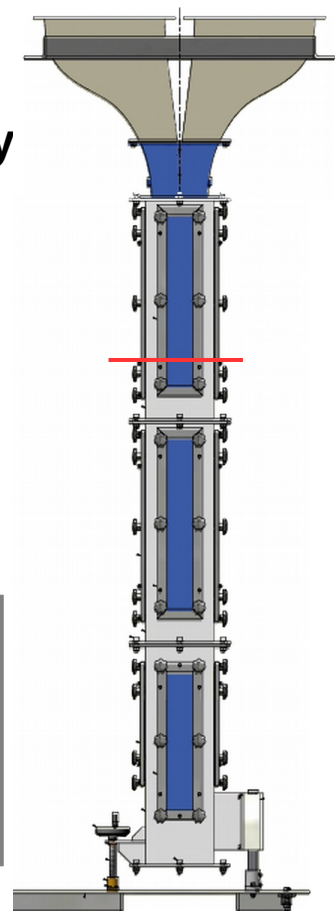
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3 Particle and droplet dynamics – Results – Medium humidity

- Comparison of particle size distribution 35cm BAI

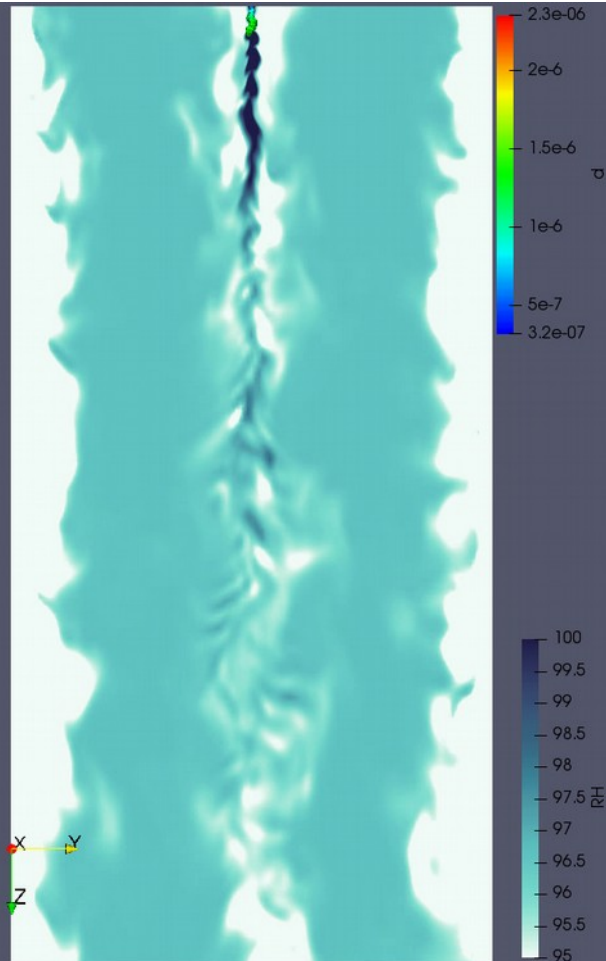


- Simulated diameter too small
- Simulated distribution too narrow
- Do BCs meet real conditions?
- Not enough time for statistics?
- Does subgrid scale turbulence play a role?

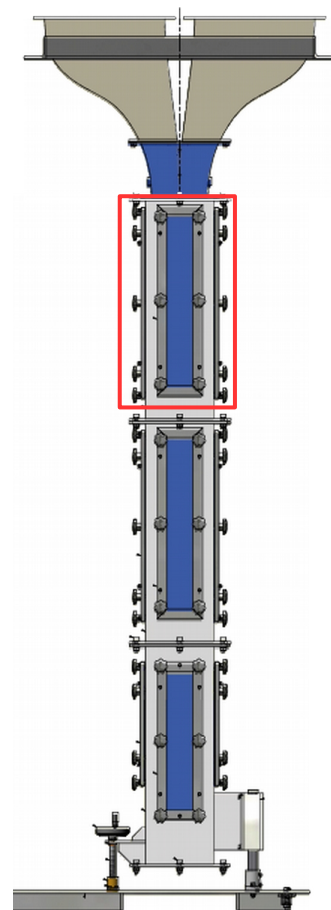
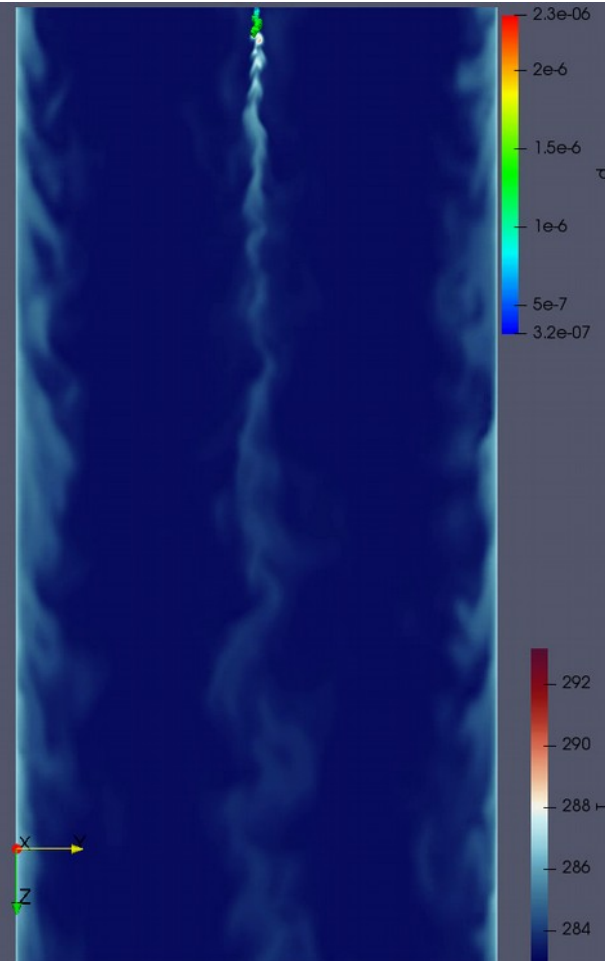


3 Particle and droplet dynamics – Results – High humidity

Relative humidity [%]



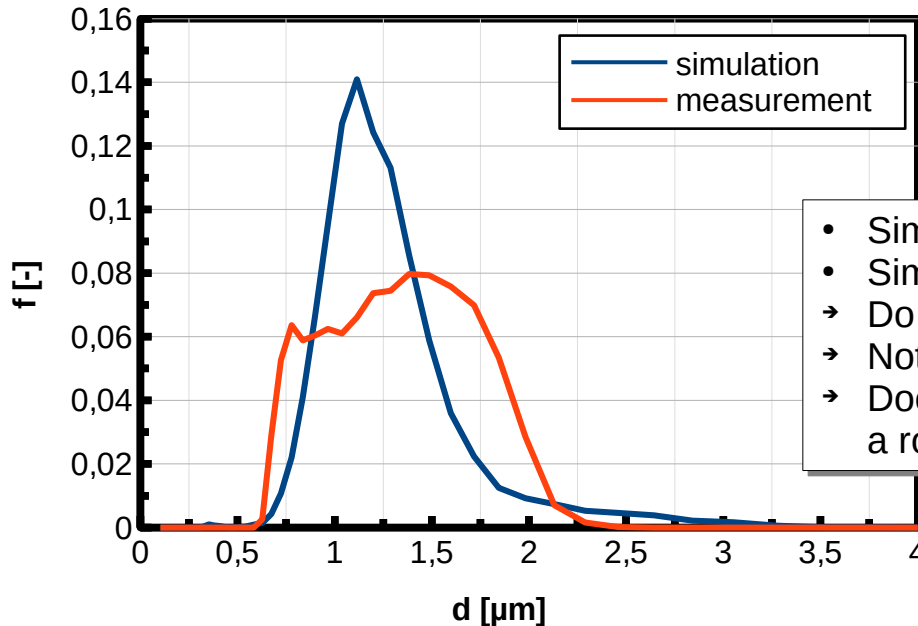
Temperature [K]



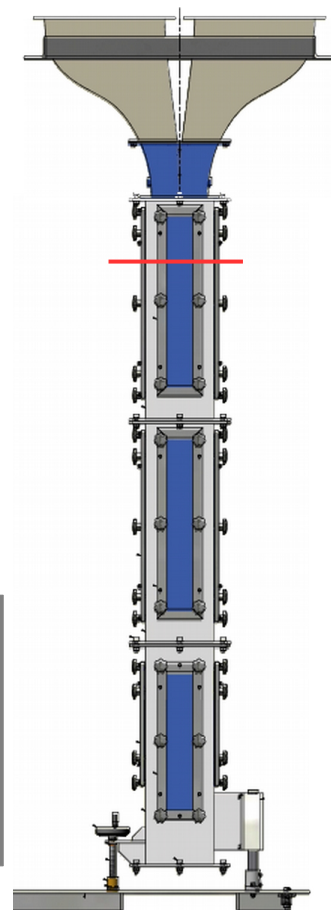
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3 Particle and droplet dynamics – Results – High humidity

- Comparison of particle size distribution 10cm BAI



- Simulated diameter okay
- Simulated distribution too narrow
 - Do BCs meet real conditions?
 - Not enough time for statistics?
 - Does subgrid scale turbulence play a role?



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4 Summary and outlook

Summary

- Simulation of flow and thermodynamics inside LACIS-T with Large Eddy Simulations
- Results agree well with measurements
- Implementation of particle growth model in OpenFOAM's Lagrangian module
- First particle simulations look promising, but have discrepancies to measurements

Outlook

- Implementation of sub grid scale turbulence dispersion for particles
- Further simulations for other conditions & longer time
- Further measurements, e.g. in lower regions of measurement section
- Long term: Correlations between turbulence and droplet/particle behaviour
- Improvements at LACIS-T (insulation, sealing) and particle measurements

Thank you for your attention!

